Influence of transparent exopolymer particles (TEP) on sinking velocity of *Nitzschia closterium* aggregates

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ABSTRACT· Sinking velocities of more than 300 Nitzschia closterium aggregates were determined during roller table incubation using digital image analysis. To examine the influence of transparent exopolymer particles (TEP) on aggregate settling speed, 3 experiments with different ratios of TEP to cell volume concentration were conducted. The results showed that, for N. closterium aggregates without TEP, sinking velocity (U) was significantly related to the equivalent spherical diameter (ESD) of the aggregates, yielding U (cm s⁻¹) = 1.89 (ESD, cm)^{0.55} The higher was the specific TEP content of an aggregate, the lower was the sinking velocity and the less pronounced was the size versus velocity relationship. Excess densities ($\Delta \rho$) of aggregates were derived from velocity measurements and 3-dimensional fractal dimensions (D3) of aggregates were calculated from scaling properties of $\Delta \rho$. Values for D3 never exceeded 2 and fit well to values of the 2-dimensional fractal dimension (D2) attained from image analysis.

KEY WORDS: Phytoplankton Aggregates · TEP · Nitzschia closterium · Sinking velocity · Fractal dimension

INTRODUCTION

In the pelagic environment the coagulation of suspended particles leads to the formation of macroscopic aggregates ('marine snow'), the sinking velocities of which can greatly exceed those of their individual components. Through their sedimentation below the surface mixed layer aggregates thus mediate the sequestration of photosynthetically fixed carbon to the ocean's interior. Since aggregation is primarily a function of particle size and concentration, the appearance of macroaggregates has commonly been observed during phytoplankton blooms (Alldredge & Gotschalk 1989, Riebesell 1991, Kiørboe et al. 1994). Species of the genus Nitzschia are common in natural macroaggregates (Cabrini et al. 1992, Passow & Alldredge 1994). The affinity of Nitzschia closterium to form aggregates has already been mentioned by Riley (1943). In laboratory experiments Monti et al. (1995) found that aged N. closterium were entangled with mucus into large stringers, similar to those found in the

Various attempts have been made to measure the settling speed of 'marine snow' in situ as well as in the laboratory. One of the main challenges in gaining accurate results has been the handling of the fragile aggregates. Herein we present a simple method for

Adriatic Sea. Mucus particles are primarily composed of acidic polysaccharides (Leppard 1995). Alldredge et al. (1993) stained polysaccharide particles with the cationic dye Alcian Blue and defined transparent exopolymer particles (TEP) on the basis of this staining capacity. Since then TEP have been shown to be abundant in many marine ecosystems (Passow & Alldredge 1994, Schuster & Herndl 1995, Hong et al. 1997, Engel 1998). The importance of TEP for the formation of aggregates is assumed to be based upon their enhancement of coagulation efficiency (Passow et al. 1994, Logan et al. 1995). In contrast to solid components of 'marine snow' like diatoms, frustules or faecal pellets, TEP are supposed to have approximately the same density as the seawater in which they are produced (Alldredge & Crocker 1995, MacIntyre et al. 1995). As a consequence TEP would enhance the formation but would reduce the sinking velocities of aggregates.

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the measurement of settling velocities of aggregates in vitro without perturbation due to isolation. Aggregates of Nitzschia closterium were formed on roller tables, and sinking rates were determined during incubation using digital image analysis. We tested the hypothesis that TEP concentration influences the sinking velocity of N. closterium aggregates by comparing results from 3 experiments ranging from low to high TEP content of aggregates.

METHODS

Theoretical considerations. The settling velocity (U_r cm s⁻¹) of a particle in fluid results from the balance between gravity force (F_a) and drag force (F_d):

$$U = [2g(\rho_{p} - \rho_{fl})V/(C_{d}\rho_{fl}A_{p})]^{0.5}$$
 (1)

where the acceleration due to gravity (g) is 981 cm s⁻², ρ is the density (in g cm⁻³), either of the particle (p) or the fluid (fl), V the particle volume, C_d the dimensionless drag coefficient and A_p the area of the particle perpendicular to the direction of the fall. For macroscopic aggregates the Reynolds numbers (Re = dU/ν , where d is the particle diameter and ν is the kinematic viscosity) are typically >0.5 and the drag coefficient must be determined empirically (White 1974). The term $\rho_p - \rho_{fl}$ denotes the excess density ($\Delta \rho$) of the particle. Excess densities of macroaggregates vary between 10^{-1} and

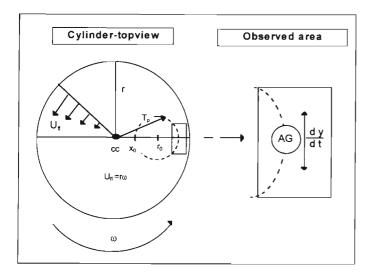


Fig. 1. Scheme of a rolling cylinder, topview. The axis (cc) of the cylinder is horizontal. Trajectories of aggregates formed on the roller table are ideally circular around the centre r_0 . The camera-observed area dissects the circular path of a particle, which is described by the trajectory vector $\mathbf{T}_{\rm p}$. In case of solid body rotation, the tangential velocity of the fluid ($U_{\rm fl}$) is a function of distance (r) to the centre (cc) of the cylinder and of the radial velocity (ω). Under this condition, the settling speed of an aggregate (AG) can be calculated from changes in vertical position

 10^{-5} g cm⁻³, which is up to 4 orders of magnitude lower than $\Delta \rho$ of single phytoplankton cells (Alldredge & Gotschalk 1988). This is due to the fact that aggregates are highly porous. Thus, the knowledge of the excess density of an aggregate is crucial to calculate its mass and consequently its settling speed.

Aggregates readily form in cylindrical tanks rotated around their horizontal axis (Shanks & Edmondson 1989). Such rotation produces a theoretical turbulence-free velocity field of the fluid (Tooby et al. 1977).

$$U_{\rm fl} = \omega r \tag{2}$$

where $U_{\rm fl}$ is the tangential velocity of the fluid (cm s⁻¹), ω is the angular velocity of the fluid (s⁻¹) and r is the radius (cm) of the cylinder (Fig. 1). The solid body rotation as described by Eq. (2) is achieved after a given spin-up time, determined as in Jackson (1994), during which the movement of the fluid propagates from the outer cylinder towards the centre. When solid body rotation is established, the trajectories of particles inside the cylinder are given by the balance between $F_{\rm g}$ and $F_{\rm d}$. Ideally, this results in closed orbital paths of particle trajectories, $T_{\rm p}(t)=(p_{\rm h},\,p_{\rm v})$, where $p_{\rm h}$ and $p_{\rm v}$ are the horizontal and vertical components of the particle trajectory vector $T_{\rm p}(t)$. If $\mathbf{X}_0=(x_0,\,0)$ is the position at time t=0, then the components of the particle trajectories can be described as:

$$p_{\rm h}(t) = (x_0 - r_0)\cos\omega t + r_0 \tag{3}$$

$$p_{v}(t) = (x_0 - r_0)\sin \omega t \tag{4}$$

At the position r_0 the quotient F_g/F_d is equal to the sinking velocity (U_0) of the particle and the sinking velocity can be considered as:

$$U_0 = \omega r_0 \tag{5}$$

Particles that have differential settling velocities collide and probably adhere, leading to the formation of aggregates.

The simultaneous measurement of aggregate size (> 10^{-3} cm) and of the appropriate orbital path (> 10^{0} cm) lacks accuracy due to the different orders of magnitude. However, during solid body rotation the sinking velocity (U) of an aggregate can also be derived from its apparent velocity (AU_{AG}):

$$U = U_{\rm v} + AU_{\rm AG} \tag{6}$$

where $U_{\rm v}$ is the vertical component of the fluid velocity at the radial distance $r_{\rm s}$ and

$$U_{v}(r) = \omega r \cos \Phi \tag{7}$$

If x denotes the horizontal axis, which intersects the centre of the cylinder (cc), then geometrical considerations give (Fig. 2):

$$x = r\cos\Phi \tag{8}$$

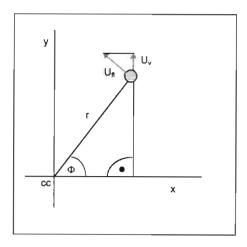


Fig. 2. Geometric illustration of Eq. (8). For $\Phi > 0^\circ$ the vertical velocity (U_v) of an object in the x-y plane is lower than the tangential velocity of the fluid $(U_{\rm fl})$ and is given by $U_{\rm v} = \omega r \cos \Phi$, with $x = r \cos \Phi$

The apparent velocity of the aggregate $(AU_{\rm AG})$ can be approximated from its vertical displacement in the x-y plane with time:

$$AU_{AG} = -\Delta y/\Delta t \tag{9}$$

To get an indication for the accuracy of the sinking velocity measurements we derived $\Delta \rho$ in our experiments from U according to Eq. (1), calculated 3-dimensional fractal dimensions (D3) from scaling properties of $\Delta \rho$ and compared them to the 2-dimensional fractal dimensions (D2) we got from the image analysis.

The excess density ($\Delta \rho$) of an aggregate is related to the density of the solid components (ρ_s) by (Alldredge & Gotschalk 1988):

$$\Delta \rho = \{ [\rho_s(1-p)] + (\rho_{fl}p) \} - \rho_{fl}$$
 (10)

where ρ_Π is the density of the fluid and p is the porosity, which is the volume fraction of the aggregate occupied by the fluid. The porosity of an aggregate is reduced if a part of the interstices is filled with TEP. It has been assumed that the density of TEP is equal to the density of the seawater in which they are produced (Alldredge & Crocker 1995, MacIntyre et al. 1995). For aggregates that settle into deeper water of higher salinity, calculation of Δp must take into account the TEP fraction inside an aggregate (Alldredge & Crocker 1995). However, since salinity did not change during the experiments of this investigation, calculation of porosity can be simplified to:

$$p = 1 - (SV/VV) \tag{11}$$

Here SV denotes the solid volume of the aggregate, which is given by the sum of volumes of the solid components, and VV is the visible volume which is occu-

pied by the aggregate. Solving Eq. (10) with Eq. (11) and assuming that ρ_s and ρ_{fl} are constant for a given type of particles, $\Delta \rho$ can be written as a function of the ratio SV/VV:

$$\Delta \rho = (\rho_s - \rho_{fl}) (SV/VV) \tag{12}$$

The solid volume of an aggregate is related to size according to (Jiang & Logan 1991):

$$SV = aI^{D3} \tag{13}$$

where l is a typical size scale and D3 is the 3-dimensional fractal dimension. So:

$$\Delta \rho \sim (al^{D3})/(bl^3) \tag{14}$$

where a and b are constants, or:

$$\Delta \rho \sim I^{D3-3} \tag{15}$$

For marine aggregates (>0.5 mm) D3 has been found to be <2 (Logan & Wilkinson 1990). Thus, Eq. (15) leads to an interpretation of an excess density that decreases with increasing aggregate size.

Diatom culture and empirical measurements. The pennate diatom *Nitzschia closterium* was isolated in November 1991 in the Kattegat by the Scandinavian Culture Centre for Algae and Protozoa (SCCAP). The algae were grown in continuous culture under 15°C, 210 μ mol m⁻² s⁻¹ photon flux in a 12 h light:12 h dark cycle and a salinity of 25. Nutrient supply was based on f/2 medium (Guillard & Ryther 1962) for Expt 1. Nitrogen limitation was found to enhance TEP production of *N. closterium* (Kraus 1997), so we chose 4 d of N-starvation for the culture used in Expt 2 and 10 d for the culture used in Expt 3.

TEP and cell volume concentrations within the aggregates were determined from samples taken after each experiment. Therefore the cylinders were carefully turned to one side, so that aggregates could settle to the bottom. Then the upper cylinder wall was removed, and aggregates were carefully isolated using a syringe with a 2 mm diameter needle.

TEP concentration was determined according to the colourimetrical method of Passow & Alldredge (1995). Three replicates of $10~\rm cm^3$ of culture and $1~\rm to~5~\rm cm^3$ of aggregate samples were filtered onto $0.4~\rm \mu m$ Nuclepore filters, stained with Alcian Blue and stored at $-21^{\circ}\rm C$ until analysis. For the microscopic observation of TEP abundance, semi-permanent slides were prepared (Passow & Alldredge 1994). Measurements of the cell volume concentration were carried out with the Coulter Counter (Coulter Multisizer II) after appropriate (<5% coincidence) dilution with $0.2~\rm \mu m$ (Nuclepore) filtered seawater. We chose the $100~\rm \mu m$ aperture, which gives accurate size measurements between 4 and $60~\rm \mu m$ equivalent spherical diameter (ESD). The sampling volume of the Coulter Counter was set to

 $2~{\rm cm}^3$, and $4~{\rm replicates}$ were measured of each sample. Since TEP cannot be detected by the Coulter Counter (Alldredge et al. 1993, authors' pers. obs.) it can readily been assumed that the volume concentration of particles $>4~{\rm \mu m}$ ESD was equal to the total cell volume concentration.

For comparison between the 3 experiments TEP concentration was related to the cell volume concentration (ϕ). This yielded a TEP: ϕ ratio of 116 \pm 0.1 μg Xanthan equivalent cm⁻³ of total cell volume for the culture of Expt 1 and 148 \pm 0.4 μg Xan. equiv. cm⁻³ and 313 \pm 0.1 μ g Xan. equiv. cm⁻³ for Expts 2 and 3, respectively (Table 1). However, in Expt 1 the microscopy showed no discrete Alcian Blue stained particles but adsorption of the dye to the cell surface. Tokuda (1969) found that the frustules of Nitzschia closterium were covered by a mucopolysaccharide sheath. Acidic polysaccharides that are bound a priori to the cell surface cannot be distinguished from TEP by the colourimetric method. So the TEP: ϕ ratio in the first experiment should be taken as a background value

All experiments on the roller table were run for 24 h at a rotation speed of 0.77 rpm. We used 2 cylinders that were 30 cm in diameter, 15 cm in height and of about 10 dm³ volume each. Aggregate position was observed with a Panasonic b/w video camera equipped with a 80 mm macro-lens placed in front of the cylinder. The observation area was 1.9×3.1 cm in size and at a distance of 9.5 cm from the centre of the tank. The camera was connected to an S-VHS videorecorder (Panasonic AG-7350) via BNC-online and recorded for 5 min every 1 to 2 h. A digital time code was placed on every video picture with a temporal resolution of 1/100 s. Video pictures were digitised on a Macintosh Power PC 7500/100 and analysed with the image program NIH-Image 160.ppc, a public domain program developed at the US National Institute of Health. The optical resolution of digitised pictures was 0.002 mm² pixel⁻¹ The following parameters of each aggregate were measured semi-automatically: topview area (A), perimeter (P), length of the major axis (major), length of the minor axis (minor), largest expansion in the horizontal direction (x-ferret length),

Table 1. TEP and cell volume concentration (6) within aggregates formed during the 3 experiments with Nitzschia closterium

| | Unit | Expt 1 | Expt 2 | Expt 3 |
|------------|---------------------------------|---------------|-------------|----------------|
| Cell volum | 277D A21 | 65.0 ± 8.69 | 26.5 ± 2.33 | 18.6 ± 2.04 |
| TE:P | µg Xam. equiv. dm ⁻³ | 7456 ± 89 | 4731 ± 5.8 | 4634 ± 229 |
| TE:P:0 | µq Xan. equiv. тт-3 | 115 ± 15 | 179 ± 17 | 249 ± 30 |

largest expansion in the vertical direction (y-ferret length) and position in the x-y plane.

The visible volume of each aggregate (VV) was calculated as the volume of an equivalent ellipsoid. The area perpendicular to the direction of fall was calculated as the maximum cross-sectional area $(A_{\rm p})$ either of a prolate or of an oblate ellipsoid. The aggregate was assumed to be prolate for y-ferret length > x-ferret length and $A_{\rm p}$ was calculated according to:

$$A_{\rm p} = \pi (\rm minor)^2/4 \tag{16}$$

Otherwise the aggregate more closely resembled an oblate ellipsoid, and A_p was calculated from:

$$A_{\rm p} = \pi (\rm major)^2/4 \tag{17}$$

The vertical velocity component $(U_{\rm v})$ of the fluid was calculated as the mean of the velocities $U_{\rm v}(x_1)$ and $U_{\rm v}(x_2)$ at the start and end position of each aggregate path. Strictly speaking this holds only if the aggregate is exactly on a circular trajectory. To be safe we ensured that $\Delta x/\Delta t << \Delta y/\Delta t$ or at least $\Delta x/\Delta t < 0.05$ $\Delta y/\Delta t$. From Eq. (5) it follows that the sinking velocity of a particle inside the cylinder may not be larger than $\omega r_{\rm max}$, otherwise the particle hits the wall of the cylinder and no 'free fall' can be measured. An observation area at the periphery of the tank was chosen to measure the higher sinking speeds of larger aggregates also.

The density of the fluid was calculated from temperature and salinity data according to the UNESCO-script of 1981.

RESULTS

Visible aggregates appeared in each roller table incubation after 2 to 3 h (Fig. 3). Consistent with the TEP: ϕ ratios of the cultures, TEP: ϕ ratios within the aggregates were lowest in Expt 1 yielding 115 ± 15 µg Xan. equiv. cm⁻³, medium in Expt 2 with 179 ± 17 µg Xan. equiv. cm⁻³ and highest in Expt 3 with 249 ± 30 µg Xan. equiv. cm⁻³ (Table 1).

Size, shape and settling velocities of more than 300 aggregates were determined. The size of all measured

aggregates ranged from 0.6 to 10 mm. Between the 3 experiments, shape and size of aggregates varied and are shown for times 5 and 10 h of incubation in Table 2. Aggregates of Expts 2 and 3, which had higher TEP: \$\phi\$ ratios, were more elongated than those of Expt 1.

Sinking velocities of all aggregates ranged from 0.34 to 1.63 cm s⁻¹ (or 301 to 1412 m d⁻¹). Sinking velocities (U_i , cm s⁻¹) of *Nitzschia closterium* aggregates

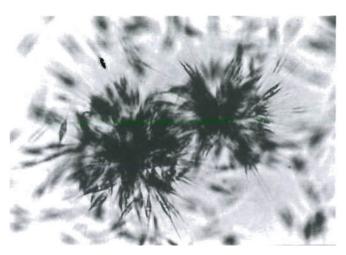


Fig. 3. Microaggregates of *Nitzschia closterium* formed during Expt 1. Cells stick directly to each other without TEP

without TEP (Expt 1) increased significantly with size (ESD, cm) following a power law function:

$$U = 1.89 (ESD)^{0.55}$$

($\rm r^2=0.68, n=139, p<0.0001$) (Fig. 4). Less pronounced yet still significant (p < 0.001) was the relationship between size and sinking velocity for aggregates of Expt 2. While for the smaller aggregates (<3 mm) a value of $U=0.72\pm0.19~\rm cm~s^{-1}$ was equal to the settling speed of smaller aggregates in Expt 1, the larger ones (>3 mm) settled more slowly ($U=0.89~\rm cm~s^{-1}$) than those of Expt 1 ($U=1.26\pm0.23~\rm cm~s^{-1}$). Sinking velocities were not related to size for aggregates of Expt 3 containing the highest TEP fraction. In contrast, the smaller aggregates (<3 mm) were found to settle at approximately the same speed (0.63 \pm 0.15 cm s⁻¹) as those >3 mm diameter (0.69 \pm 0.08 cm s⁻¹).

To calculate $\Delta \rho$ according to Eq. (1), we used White's (1974) empirically derived formula for the drag coefficient at higher Reynolds numbers, because the Reynolds numbers we derived for aggregates from measurements of velocity, size and fluid viscosity

Table 2. Size and shape of aggregates formed during roller table incubation. Given are the mean values (median) of data obtained from Expts 1 to 3 after 5 and 10 h of incubation (VV: visible volume of an aggregate; Min.:Maj.: ratio of minor axis to major axis of an aggregate)

| | Expt 1 | | Expt 2 | | Expt 3 | |
|--|----------------------|---------------------|----------------------|---------------------|----------------------|---------------------|
| | 5 | 10 | 5 | 10 | .5 | 10 |
| n | 29 | 24 | 9 | 29 | 12 | 26 |
| Major (μm) VV (mm ³) Min.:Maj. | 1238 0.44 0.70 | 1842 1.8 0.72 | 1053 0.27 0.66 | 1922 1.6 0.66 | 1119 0.21 0.54 | 2032 1.3 0.54 |

exceeded the threshold value of 0.5 for Stokes settling in every case (Fig. 5)

Excess densities of measured aggregates covered 2 orders of magnitude and ranged from 8.8×10^{-2} to 9.5×10^{-4} g cm⁻³. In each experiment $\Delta \rho$ decreased with size of aggregates (Fig. 6). On the basis of Eq. (15) a power law function for $\Delta \rho = a l^b$

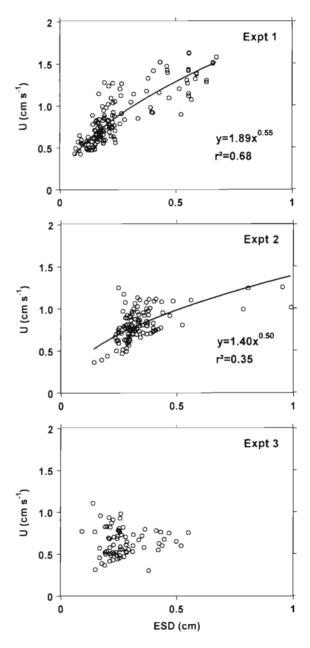


Fig. 4. Relation between sinking velocity $(U, \text{ cm s}^{-1})$ of *Nitzschia closterium* aggregates and the equivalent spherical diameter (ESD, cm). Sinking velocity of aggregates without TEP (Expt 1) was highest and increased with size following a power law function (n = 139, p < 0.0001). Correlation between U and ESD was less pronounced in Expt 2 (n = 112, p < 0.001) and absent in Expt 3 (n = 74, ns)

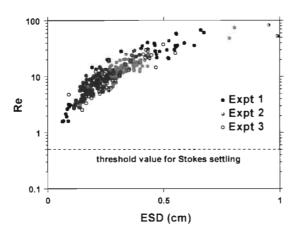


Fig. 5. Reynolds numbers (Re) of *Nitzschia closterium* aggregates, calculated from size, sinking velocity and fluid viscosity data, exceeded the threshold value of 0.5 for Stokes settling and increased with the equivalent spherical diameter (ESD, cm) of the aggregates

was assumed with l= major and b= D3 – 3. Decrease of $\Delta \rho$ with the major axis of aggregates was steepest for aggregates of Expt 3 and lowest for aggregates of Expt 1. Linear regression of log $\Delta \rho$ versus log major yielded a slope of $b_1=-1.03\pm0.049,\ b_2=-1.27\pm0.073$ and $b_3=-1.56\pm0.075$ for Expts 1, 2 and 3, respectively.

Values of D3 for aggregates of Expts 1, 2 and 3 were $\mathrm{D3}_1 = 1.97 \pm 0.049$, $\mathrm{D3}_2 = 1.73 \pm 0.073$ and $\mathrm{D3}_3 = 1.44 \pm 0.075$, respectively. Therefore, the assumption D3 < 2 was confirmed for aggregates of *Nitzschia closterium*. For an ideal, infinite fractal, D3 equals the 2-dimensional fractal dimension (D2) if D3 < 2 (Meakin 1988). Hence, the comparison of values of D3 and D2 can be used to test whether D3 derived from sinking velocity measurements are reliable. As D3 expresses the scaling relationship between length and solid volume of an aggregate, D2 can be derived relating length to area according to (Kilps et al. 1994):

$$A \sim l^{D2}$$

D2 of aggregates in our experiments was attained by calculating the slope of the linear regression, log(A)

Table 3. Two- (D2) and 3-dimensional (D3) fractal dimensions of *Nitzschia closterium* aggregates (Expts 1 to 3) (CI: confidence interval; n: number of aggregates used for regression analysis)

| Expt | n | D3 CI (95%) r ² D3 ± | | | D2 CI (95%) r ² D2 ± | | |
|------|-------|------------------------------------|------|------|------------------------------------|------|------|
| 1 | 139 | 1.97 | 0.13 | 0.87 | 1.96 | 0.01 | 0.95 |
| 2 | 1.1.2 | 1.73 | 0.19 | 0.73 | 1.72 | 0.01 | 0.87 |
| 3 | 34 | 1.44 | 0.20 | 0.87 | 1.44 | 0.01 | 0.92 |

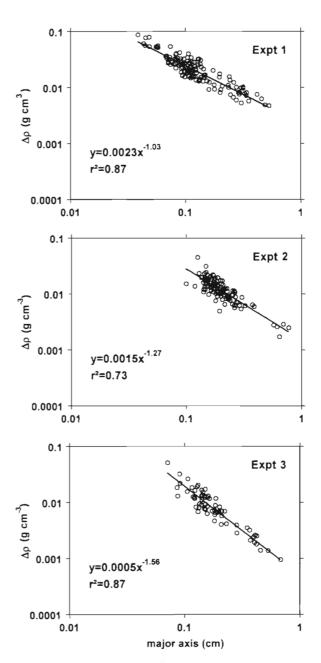


Fig. 6. Decrease of Δp (g cm⁻³) with the major axis (cm) of Nitzschia closterium aggregates, without TEP (Expt 1), with medium TEP content (Expt 2) and with high TEP content (Expt 3)

versus log (major), whereby measurements of area and major were performed on the same aggregates as sinking velocity determinations. A 95% confidence interval was prescribed for D3 = (b + 3) and for D2 (Table 3). For each experiment the value of D3 lies within the confidence interval of D2 and vice versa. Thus there were no statistically significant differences between the independently determined values of D3 and D2 (p < 0.05).

DISCUSSION

Various previous studies have stressed the important role of marine aggregates in the vertical transport of particulate matter (Shanks & Trent 1980, Asper et al. 1992). To calculate particle flux, information is needed on time scales of sedimentation as well as on the variability of settling velocity due to compositional changes. We have proposed a method, based on the determination of settling velocity inside the rolling cylinder via image analysis, to elucidate these parameters.

Aggregate excess density derived from velocity measurements was reproducible from the theoretical approach with fractal dimensions. So the presented method for the measurement of aggregate settling velocity is a suitable alternative, e.g. to settling chambers, for it does not require the isolation of aggregates and enables the simultaneous determination of size, shape and settling speed of a large number of aggregates.

The fractal properties of aggregates provide information on the size to volume scaling relationship and on the mechanisms of the coagulation process (Meakin 1991). Previously reported 2- and 3-dimensional fractal dimensions of marine snow are in the range of 1.39 to 1.81 (Logan & Wilkinson 1990, Kilps et al. 1994, Chen & Eisma 1995, Li & Logan 1995), which corresponds to the fractal dimensions determined for Nitzschia closterium aggregates in Expt 2 and Expt 3 of the present study. We found that D3 of aggregates derived from velocity measurements were in good accordance with values of D2 determined by image analysis on their projection. This corroborates the applicability of image analysis for the examination of the fractal nature of aggregates, which is especially useful for the interpretation of in situ photographs.

Absolute values of sinking velocity of Nitzschia closterium aggregates determined during this study were higher than sinking velocities of diatom flocs measured in situ (Alldredge & Gotschalk 1988). Lower sinking speed of natural aggregates may result from several factors. First, natural flocs are more heterogeneous and may contain particles with a lower density than diatoms. Second, excess densities of N. closterium aggregates ranged from 10^{-2} to 10^{-4} g cm⁻³, which is up to 2 orders of magnitude higher than values obtained for natural flocs (Alldredge & Gotschalk 1988, Diercks & Asper 1997). Of course aggregates with high excess density can hardly achieve large size in the water column. They would rapidly settle out at small stages. The rolling cylinder is a closed system in which aggregation can continue as long as particle concentration is high enough to permit sufficient particle contact rates. The initial cell concentration of *N. closterium* cultures used here was much higher than natural abundance of diatoms. However, the primary goal of this investigation was to compare the relative effects of different TEP contents on aggregate settling velocity rather than the measurement of absolute sinking speeds applicable to nature. Sinking velocities determined for aggregates that were formed from natural water samples, using the same method as this study, were much lower and more comparable to previously reported values (Engel 1998). However, Lick et al. (1993) found that aggregates which are produced via differential settlement, like on the roller table, sink faster than aggregates produced by fluid shear.

Regarding the influence of TEP on the settling velocity of *Nitzschia closterium* aggregates, the 2 different methodological approaches gave consistent results. (1) Aggregates without TEP had higher values of fractal dimension, excess density and consequently higher settling velocities than aggregates with TEP. (2) The higher was the TEP: ϕ ratio of an aggregate, the lower were the values of D3, $\Delta \rho$ and U.

TEP apparently affect the vertical flux of particulate matter in 2 ways: on the one hand they enhance aggregate formation due to their high stickiness (Passow et al. 1994, Dam & Drapeau 1995). On the other hand they reduce the settling velocity and consequently the export rates of aggregates by decreasing the excess density.

Variability of aggregate settling velocity with size due to compositional differences is well documented in the literature (see Alldredge & Silver 1988 for review). Previous studies which showed the existence of a relationship between aggregate size and settling velocity yielded different empirical functions, e.g. $U = 0.67d^{0.57}$ (Kajihara 1971), $U = 50d^{0.26}$ (Alldredge & Gotschalk 1988) and $U = 0.64 d^{1.25}$ (Lick et al. 1993). We found that incorporation of TEP into aggregates modulates the size versus velocity relationship and may even abolish it. This may be helpful for the interpretation of in situ observations, which showed that size of natural aggregates was not related to settling velocity (Diercks & Asper 1997). However, more information concerning the temporal and spatial role of TEP within aggregates will be needed, e.g. for numerical ecosystem models which include the aggregation process for better estimates of the vertical biomass flux.

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